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# Liquid Transfer for Viscoelastic Solutions

Hrishikesh Pingulkar, Jorge Peixinho,\* and Olivier Crumeyrolle

**ABSTRACT:** Viscoelastic liquid transfer from one surface to another is a process that finds applications in many technologies, primarily in printing. Here, cylindrical-shaped capillary bridges pinned between two parallel disks are considered. Specifically, the effects of polymer mass fraction, solution viscosity, disk diameter, initial aspect ratio, final aspect ratio, stretching velocity, and filling fraction (alike contact angle) are experimentally investigated in uniaxial extensional flow. Both Newtonian and viscoelastic polymer solutions are prepared using polyethylene glycol and polyethylene oxide, with a wide variety of mass fractions. The results show that the increase in polymer mass fraction and solvent viscosity reduces the liquid transfer to the top surface. Moreover, the increase in the initial and final stretching heights of the capillary bridge also decreases the liquid transfer for both Newtonian and viscoelastic solutions. Finally, the shape of the capillary bridge is varied by changing the liquid volume. Now, Newtonian and viscoelastic solutions exhibit opposite behaviors for the liquid transfer. These findings are discussed in terms of interfacial shape instability and gravitational drainage.

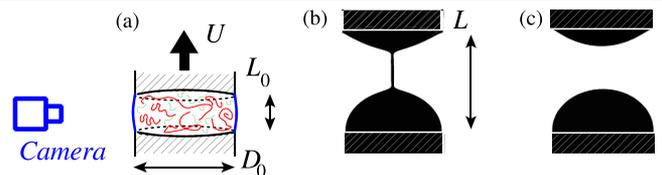


## INTRODUCTION

Liquid capillary bridges can be found in many industrial applications such as food processing, material engineering, adhesion processes, coating technology, flow in porous media, microfluidics, and measurements of rheological properties.<sup>1-4</sup>

One of the motivations for the study of stretched liquid bridges is its close association with printing processes. Nowadays, a printing process not only is limited to books, magazines, and newspapers but also has expanded to various areas like manufacturing of electric circuits,<sup>1</sup> printed wearable electronics,<sup>5</sup> screen displays, lab-on-a-chip,<sup>6</sup> solar cells,<sup>7</sup> and 3D microstructures (polymer wires, needles, pillars, cones, and microspheres).<sup>8</sup> The printing industry deals with inks, which can contain polymers, surfactants, or particles and have viscoelastic properties. While printing, the liquid from one surface is transferred to another surface through the formation of a capillary liquid bridge. For Newtonian fluids, during this liquid transfer, solution pools are formed on the end plates of a stretched liquid bridge. On the other hand, a stretched viscoelastic liquid bridge forms a persistent thin filament<sup>9-14</sup> along with the solution pools.

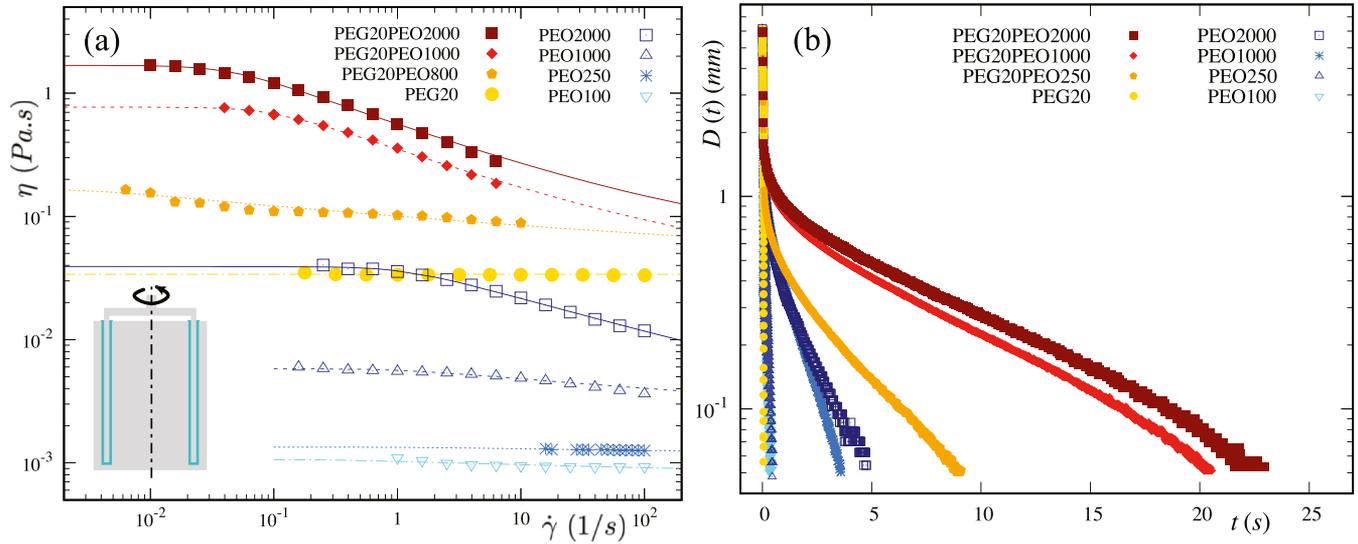
Due to complexities involving surface and liquid properties as well as the formation of filaments, the transfer of the desired volume of liquid is a challenge in the printing industry. Specifically, capillary, viscous, inertial, elastic, and gravitational forces all play a role in this liquid transfer. A relevant parameter called the transfer ratio,  $T_r$ , is defined as the fraction of liquid transferred to the moving disk (accepter) to the total amount of liquid left on both disks, as shown in Figure 1. The geometrical properties that affect  $T_r$  are the disk radius,  $R_0$ , or



**Figure 1.** (a) Liquid capillary bridge of the polymer solution sandwiched between parallel disks of diameter  $D_0$  and initial height  $L_0$  before being stretched with a velocity,  $U$ . (b) The top disk reaches the final stretching height,  $L$ , and a thinning filament is observed. (c) Breakup of the liquid bridge.

the disk diameter,  $D_0$ , the stretching speed,  $U$ , the initial aspect ratio,  $L_0/R_0$ , and the final aspect ratio,  $L/R_0$ .

Chadov and Yakhnin<sup>15,16</sup> first identified the liquid-transfer phenomenon for several liquids of viscosity  $\eta$  and surface tension  $\sigma$  on various surfaces. In their experiments, the top flat surface was brought downward to press a liquid drop on the bottom surface and then moved upward to stretch the capillary bridge at high capillary numbers, that is,  $Ca = \eta U/\sigma > 1$ . Under these conditions, the liquid transfer is independent of surface and liquid properties, which was later confirmed by others authors.<sup>17-20</sup> Noteworthy, when the contact angles on both plates are  $45^\circ$ ,  $T_r$  is found to be 0.5.



**Figure 2.** (a) Steady shear viscosity against shear rate and (b) diameter time evolution for aqueous solutions of PEO, PEG, and PEG20PEO. The inset in (a) is a sketch of the double-wall geometry (drawn up to scale) used, and the lines represent fits described in the text.

The issues of wetting and the dynamic contact angle<sup>21</sup> are generally avoided by pinning the contact line to the edge of a disk. For example, Zhang et al.<sup>22</sup> investigated, theoretically and experimentally, the stability and breakup of the liquid bridge, with fixed contact lines at the edges. The authors found that  $T_r$  decreases with increasing disk diameter but increases with the stretching speed. In practice, gravure cells are used<sup>23–26</sup> to control the ink spreading. The effect of viscoelastic polymer solutions on  $T_r$  for the gravure printing is studied experimentally by Sankaran and Rothstein<sup>25</sup> and numerically by Lee et al.<sup>26</sup> In the beginning, the liquid transfer is governed by the early stretching dynamics, while the final amount of liquid transfer occurs through the delayed viscoelastic filament thinning.<sup>25–27</sup> In contrast, the present study focuses on the cylindrical-shaped liquid bridges, with the pinned contact lines on disks to overcome the shearing effect.<sup>27</sup>

In the present paper, our experimental study mainly focuses on  $T_r$  for a cylindrical-shaped bridge of viscoelastic as well as Newtonian fluids. Solutions will be prepared by varying the mass fraction and molecular weight of polymers to investigate the effect of viscoelasticity on liquid transfer. The same stainless-steel disks at the top and bottom will be used to overcome the complexities due to different surface materials as previously reported.<sup>15,16,27</sup> Different disk diameters, initial and final aspect ratios, and the initial profile curvatures are explored.

## MATERIALS AND METHODS

**Sample Preparation.** Aqueous solutions of poly-ethylene oxide (PEO), which is a high-molecular-weight polymer, and poly-ethylene glycol (PEG), which has a relatively low molecular weight, are used either separately or in combination. PEO solutions are commonly used to investigate viscoelastic behavior of liquid jets,<sup>28,29</sup> beads on a string,<sup>10,14,30,31</sup> coatings,<sup>32–34</sup> and liquid transfer.<sup>25,27</sup> Broadly, our strategy is to control the shear viscosity with PEG and the extensional viscosity with the mass fraction of PEO. The molecular weight of PEO is  $8 \times 10^6$  g/mol and the molecular weight of PEG is 20,000 g/mol according to Sigma-Aldrich. Three different types of solutions are prepared: (i) aqueous PEG solutions, (ii) aqueous PEO solutions, and (iii) mixtures of PEG and PEO solutions. For the solutions containing PEO, 0.5 wt % iso-propyl alcohol is added for easy dispersion of PEO molecules in the solvent.<sup>35</sup> The mass fraction of PEO in solutions

ranges from 100 to 2000 ppm with and without PEG. Note that a solution of 1000 ppm of PEO is labeled as PEO1000. Similarly, a solution of 20 wt % PEG and 2000 ppm of PEO is labeled as PEG20PEO2000. The density,  $\rho$ , and  $\sigma$  were measured for each solution, and the values are reported in Table S1 in the [Supporting Information](#).

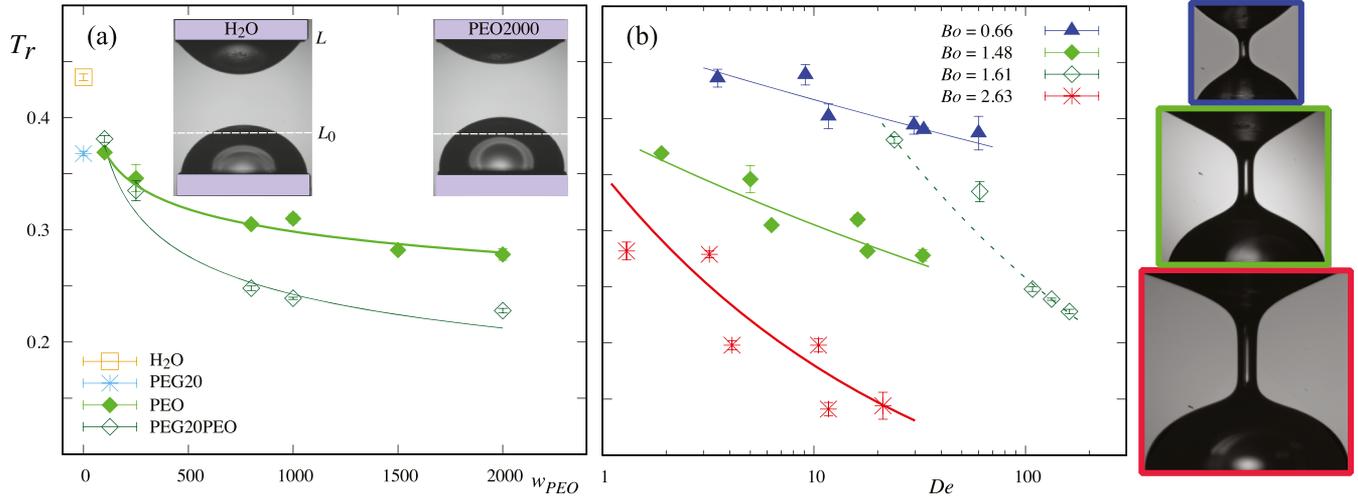
**Rheological Measurements.** The shear viscosity of the solutions was measured using a rotating rheometer (TA Instruments Discovery HR-3) with a double-wall concentric cylinder geometry. High-polymer-mass-fraction solutions exhibit shear thinning, as shown in [Figure 2a](#). The zero shear viscosity,  $\eta_0$ , was obtained from fitting the Carreau equation<sup>36</sup> with the infinite viscosity prescribed to the solvent one.

Additional rheological measurements were conducted using a capillary breakup extensional rheometer (CaBER from Thermo Haake). The filament diameter around mid-height is tracked over the time using an in-built laser (see [Figure 2b](#)). The diameter decreases with time for all solutions. For viscoelastic solutions, the diameter exhibits an exponential thinning, characterized by the extensional relaxation time,  $\lambda$ . Further analysis of the diameter can be used to obtain the extensional viscosity as a function of time and Hencky strain. These results are given in Pingulkar et al.<sup>14</sup>

Based on the solution properties, several dimensionless numbers can be defined. The Deborah number,  $De = \lambda/\tau_R$ , represents a ratio of the viscoelastic time,  $\lambda$ , to the Rayleigh inertio-capillary time:

$\tau_R = \sqrt{\rho R_0^3/\sigma}$ . Other authors<sup>26,37</sup> use the ratio  $\lambda/\tau_v$  with the viscous time  $\tau_v = \eta_0 R_0/\sigma$ . In addition, the ratio of the viscous and Rayleigh times is also needed, that is, the Ohnesorge number:  $Oh = \tau_v/\tau_R$ . Another important number to characterize a capillary bridge is the Bond number quantifying the effect of gravitational to capillary forces:  $Bo = \rho g R_0^2/\sigma$ . Later, when the capillary bridge shape is non-cylindrical, the mid-height radius,  $R_{mid}$ , will be used, leading to  $Bo_m$ . The experiments use three disk diameters and additional mass fractions, and parameters are presented in Table S2 in the [Supporting Information](#).

**Experimental Setup.** The capillary bridge stretching is studied experimentally with the CaBER and a high-speed camera ( $800 \times 1280$  pixels). The resolution for typical experiments is 1 pixel = 2  $\mu\text{m}$ . Shadowgraphic images are obtained using a continuous laser and a diffuser (from Dantec Dynamics). Initially, a liquid capillary bridge is created by placing a solution sample in between the two parallel disks. The volume of the solution introduced in the liquid bridge depends on  $R_0$  and the initial height,  $L_0$ , and this volume is calculated as  $\mathcal{V} = \pi L_0 R_0^2$ . The liquid volume introduced is controlled with the



**Figure 3.** (a) Transfer ratio,  $T_r$ , as a function of the polymer mass fraction,  $w_{PEO}$ .  $R_0 = 3$  mm,  $L_0/R_0 = 0.66$ , and  $L/R_0 = 2$  at  $U = 0.08$  m/s. (b) Transfer ratio,  $T_r$ , as a function of  $De$  for different  $Bo$ . The insets are stretched liquid bridges for 1000 ppm of PEO for  $R_0 = 2, 3,$  and  $4$  mm (from top to bottom).

help of a pipette (Eppendorf research plus). After stretching of the liquid bridge, solution pools are formed on the top and bottom disks, as shown in the binarized image in Figure 1c. Considering the axisymmetric capillary bridge, images of the vertical cross-section of the solution pools are captured. Then, heights,  $h_T$  and  $h_B$ , of top and bottom solution pools, respectively, are estimated by counting the pixels in the appropriate directions. The truncated sphere method<sup>17</sup> is implemented to calculate the volume of the solution pools:  $V_{T,B} = \pi h_{T,B}(3R_0^2 + h_{T,B}^2)/6$ . Therefore, the transfer ratio,  $T_r$ , is defined in the same way as previous authors<sup>16,17,20,38,39</sup> as  $T_r = V_T/(V_T + V_B)$ . In the following, every  $T_r$  data point and the associated error bar symbolize the average of five experiments and their dispersion, respectively.

## EXPERIMENTAL RESULTS AND DISCUSSION

The results consist of a series of experiments that report the  $T_r$  for different polymer mass fractions, disk diameters, final heights, and finally different shapes of the initial capillary bridge. The resulting  $T_r$  are discussed in terms of morphology of the interface and gravitational drainage.

**Effect of Polymer Mass Fraction.** The PEO mass fraction is varied, in the aqueous PEO and PEG + PEO solutions, to test its influence on  $T_r$ . Experiments are performed using water, PEG20, PEO, and PEG + PEO solutions. For these experiments, cylindrical-shaped initial liquid bridges are prepared with  $R_0 = 3$  mm and  $L_0/R_0 = 0.66$ . Then, the liquid bridges are stretched to  $L/R_0 = 2$  at  $U = 0.08$  m/s. These initial capillary bridges are inside the stability limit curve.<sup>40</sup> The  $T_r$  obtained are presented against the PEO mass fraction,  $w_{PEO}$ , in Figure 3a. For both the PEO and PEG + PEO solutions,  $T_r$  decreases with increasing  $w_{PEO}$ . The same can be confirmed from the inset photographs where a smaller top solution pool for PEO2000 solution compared to water can be observed.

Typically, for a viscoelastic liquid bridge, the liquid transfer occurs in two stages. In the first stage, when a liquid bridge is stretched, the minimum radius location along the filament appears and an initial liquid transfer takes place from the bottom to the top disk. When  $Bo > 1$  for  $R_0 = 3$  mm (see Table S2 in the Supporting Information), an initial asymmetry (sagging) decides the primary liquid distribution along the stretched liquid bridge. Hence, when the liquid bridge is stretched, initially, a larger bottom solution pool is formed compared to the top solution pool. However, for PEO and PEG + PEO solutions, solution pools are formed along with a filament that plays a significant role in the second stage of liquid transfer. In this second stage, the liquid is transferred from the top to the bottom solution pool due to gravitational drainage through the filament. As observed in Figure 2b, with increasing  $w_{PEO}$ , the filament lasts longer and liquid

bridge rupture gets delayed.<sup>32</sup> As a result, there is more time for the gravitational drainage and more liquid is transferred from the top to the bottom solution pool. For a low mass fraction, for both PEO and PEG + PEO solutions, the filament breaks up early and there is less time available for the liquid transfer from the top to the bottom solution pool. Hence, the viscoelastic liquids nearly reproduce the response of PEG20, as reported by Sankaran and Rothstein.<sup>25</sup> Furthermore, for PEG + PEO solutions, the filament lasts longer compared to the PEO solutions. Hence, because of the higher gravitational drainage, lower values of  $T_r$  are obtained for the PEG + PEO solutions compared to the PEO solutions. Power law fits are used to capture the change in  $T_r$  with  $w_{PEO}$ , and the exponents for PEO and PEG + PEO solutions are 0.09 and 0.19, respectively. The larger exponent of the fit for the PEG + PEO solutions than for the PEO solutions suggests that the effect of change in  $w_{PEO}$  is higher for the PEG + PEO solutions.

Furthermore, for PEO and PEG + PEO solutions,  $T_r$  is plotted as a function of  $De$  in Figure 3b. For both solutions,  $T_r$  decreases with increasing  $De$ . Similar behavior was observed numerically by Lee et al.,<sup>26</sup> where the authors reported that the liquid transferred to the top disk decreases with an increase in  $De$ . However, these results were obtained for a combination of the gravure cell at the bottom and a flat plate moving upward. Again, power law fits can be used to represent  $T_r$ , and the exponents differ for PEG + PEO solutions ( $-0.27$  for  $Bo = 1.61$ ) compared to PEO solutions ( $-0.10$  for  $Bo = 1.48$ ).

**Effect of Disk Radius.** One of the important parameters of the capillary bridge geometry is the disk radius. To understand the influence of  $R_0$  on  $T_r$ , disks of different radii, such as 2, 3, and 4 mm, are tested by keeping other geometric parameters the same. As a result, depending on  $R_0$ , the Bond number,  $Bo$ , varies from 0.66 to 2.63. For these set of experiments,  $L_0/R_0$  and  $L/R_0$  are kept constant at 0.66 and 2, respectively, whereas the stretching speed,  $U$ , is again 0.08 m/s. It can be observed that for all disk radii tested,  $T_r$  decreases with  $De$ . Additionally, the increase in  $R_0$  as well as  $Bo$  globally leads to the decrease in  $T_r$  and indicates the effect of gravity. A similar decrease in  $T_r$  with  $R_0$  has been reported for water by Zhang et al.<sup>22</sup>

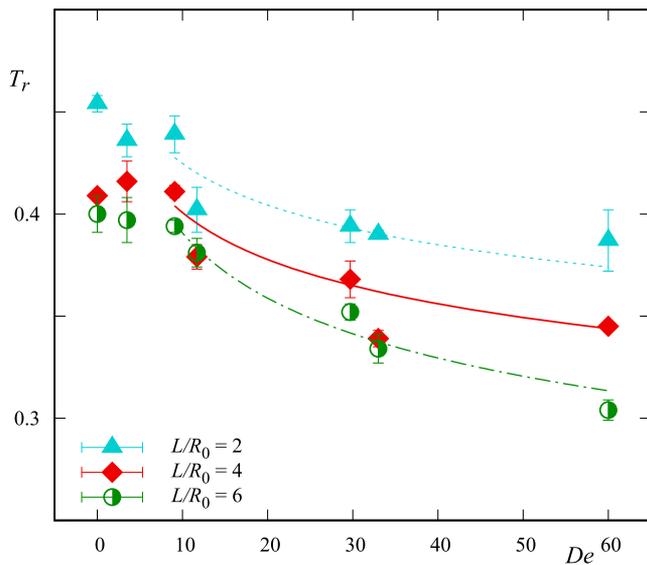
In the photographs of Figure 3b, the stretched liquid bridges with different  $R_0$  are displayed for PEO1000 solution at  $L/R_0 = 2$ . With an increase in  $R_0$  from 2 to 4 mm, the shape of the top solution pools weakly changes from convex to concave in the vertical plane, but the shape of the bottom solution pools remains convex. However, the capillary pressure associated to the shape change is dominated by hydrostatic pressure difference ( $\rho g L$ ). In addition, for the largest  $R_0$ , the hydrostatic pressure difference overcomes the capillary pressure associated to the mean curvature in the horizontal planes of the top solution pool. Hence, with increasing  $R_0$ , more solution is pushed

from the top solution pool toward the bottom solution pool due to the increased stretched liquid bridge height (fixed  $L/R_0 = 2$ ). Furthermore, it has been observed that the filament thinning time increases with increasing  $R_0$ . Hence, the gravitational drainage through the filament is enhanced by the larger disk radius that results in lower values of  $T_r$ . For each  $Bo$ , power law fits are again used to capture the change in  $T_r$  with  $De$ . With increasing  $Bo$ , the power law exponents increase from 0.05 to 0.29, suggesting a larger effect of  $De$  on higher  $Bo$  due to the combined effect of gravity and delayed filament thinning. For each  $w_{PEO}$ ,  $T_r$  decreases linearly with  $Bo$ . A reduced plot is shown in the Supporting Information (Figure S1b).

**Effect of Final Stretching Height.** The effect of the final stretching height on the liquid transfer is explored by varying the final aspect ratio,  $L/R_0$ , from 2 to 6. All other geometrical and stretching parameters are kept constant. The minimum value of  $L/R_0$  is limited by the least value of the stretching height required for breaking of the capillary bridge, whereas the maximum value of  $L/R_0$  is limited by the experimental constraints. Two different experimental studies are carried out for the PEG20 and PEO solutions.

**PEG20 Solution.** The obtained results for the variation of  $T_r$  are plotted against  $L/R_0$  in Figure S3 in the Supporting Information. The photographs illustrate different shapes of the capillary bridges formed, just before their breakup, when the top disk is at  $L/R_0 = 2, 4$ , and 6. The  $T_r$  decreases linearly with an increase in the  $L/R_0$ . For  $L/R_0 = 6$ , the breakup occurs close to the top solution pool, compared to the breakup at the middle of the bridge, for  $L/R_0 = 2$ . This further suggests that after breakup, the liquid transferred to both disks will be nearly the same for  $L/R_0 = 2$ . However, with increasing  $L/R_0$ , as the breakup point moves closer to the top solution pool, more liquid volume will be enclosed below this breakup point and a larger solution pool is formed on the bottom disk. Hence, with increasing final stretching height, less liquid will be transferred to the top disk.

**PEO Solutions.** The change in  $T_r$  for values of  $L/R_0 = 2, 4$ , and 6 is plotted against  $De$ , as shown in Figure 4. For all  $L/R_0$ , with the



**Figure 4.**  $T_r$  as a function of  $De$  for different  $L/R_0$  using PEO solutions. The liquid bridge, formed in between the two disks having  $R_0 = 2$  mm is stretched from  $L_0/R_0 = 0.66$  to different  $L/R_0$  at  $U = 0.08$  m/s.

increase in  $De$ ,  $T_r$  decreases. Additionally, for the same  $De$ , it can be noted that the increase in  $L/R_0$  leads to the decrease in  $T_r$ . This behaviour appears to be more significant for  $De > 10$ . Hence, for  $De > 10$ , power law fits of  $T_r$  are used for each  $L/R_0$ . With increasing  $L/R_0$ , the value of the power law exponent increases from 0.07 to 0.12. The location of the necking points, on the liquid bridge, varies with different  $L/R_0$ , in a similar manner to PEG20 (see photographs in

Figure S3 in the Supporting Information). The length of the filament increases with increasing  $L/R_0$ , and hence, a larger liquid volume is enclosed below this necking point. Again, the filament lasts longer with the increase in  $De$ , which further helps for the drainage. This combined effect of the location of the necking point and drainage produces smaller values of  $T_r$  at higher  $L/R_0$  and  $De$ .

Effects of stretching speed on liquid transfer are discussed in detail in the Supporting Information, in Figure S4. For PEO solutions, our results show that  $T_r$  does not increase significantly with increasing  $U$  due to  $Ca \leq 0.01$ .

**Effect of Initial Bridge Shape.** The influence of initial bridge shape on liquid transfer is studied by varying the liquid volume introduced with the pipette. This also plays a role in setting the initial liquid contact angles. For a cylindrical-shaped liquid bridge, the liquid volume is  $\mathcal{V}$ . Then, a dimensionless parameter,  $\bar{V}$ , is defined as the ratio of the actual liquid volume introduced to  $\mathcal{V}$ . The cylindrical-shaped liquid bridge, for which  $\bar{V} = 1$ , and the associated contact angle on the top disk,  $\theta_T \simeq 90^\circ$ , are illustrated in the inset of Figure 5a.  $\bar{V}$  is varied from 0.5 to 1.25, resulting in  $55^\circ \lesssim \theta_T \lesssim 115^\circ$ . In our experiments, for  $\bar{V} < 0.5$  or  $\bar{V} > 1.25$ , the bridge is found to be unfeasible or unstable.

Four different types of fluids, such as water, PEG20, PEO1000, and PEG20PEO1000, are used to characterize the effect of the initial bridge shape on  $T_r$ . The liquid bridges, formed with  $R_0 = 2$  mm, are stretched from  $L_0/R = 0.66$  to  $L/R = 2$  at  $U = 0.134$  m/s. The initial bridge shape with the contact angles,  $\theta_T < 90^\circ$ , at the top disk is similar to those in previous works,<sup>17,18,27,38</sup> where slipping contact lines were observed. However, in our case, the liquid contact lines are pinned for all initial bridge shapes. The aqueous solutions have the tendency to wet the hydrophilic stainless-steel disks. Clearly, PTFE disks would lead to unpinning and sliding of the contact lines, which in turn induce unwanted interface dynamics<sup>1,27</sup> in the present study. The obtained  $T_r$  results are plotted against the increasing  $\bar{V}$  in Figure 5a. It can be observed that  $T_r$  increases with an increase in  $\bar{V}$  for water and PEG20. However, for PEO1000 and PEG20PEO1000 viscoelastic solutions, the increase in  $\bar{V}$  has exactly the opposite effect, where  $T_r$  decreases with an increase in  $\bar{V}$ .

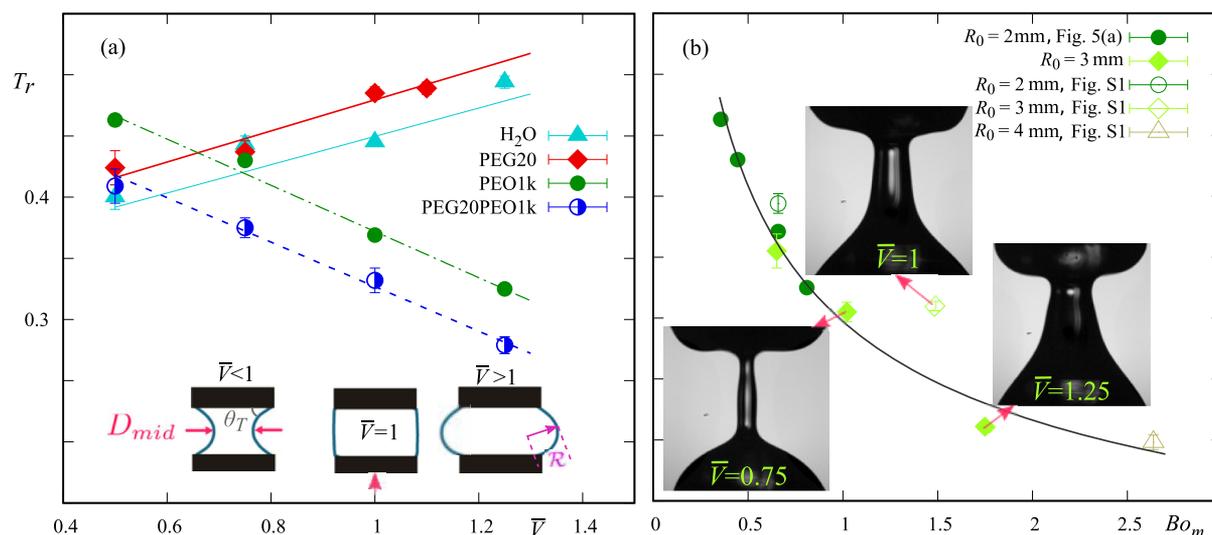
The effect of the initial bridge shape is further investigated, for PEO1000, by measuring the mid-plane diameter,  $D_{mid}$ , of the initial liquid bridge, for  $R_0 = 2$  and 3 mm, for all  $\bar{V}$  using image analysis. The inset photographs illustrate different shapes of PEO1000 liquid bridges formed for various  $\bar{V}$  with  $R_0 = 3$  mm when the top disk is at  $L/R_0 = 2$ . With an increase in  $\bar{V}$ , a larger filament radius can be observed, which enhances the gravitational drainage through the filament. Note that this filament radius after stretching is related to  $R_{mid}$ . Then,  $T_r$  is plotted in Figure 5b against the modified Bond number calculated using  $R_{mid}$  that is,  $Bo_m = \rho g R_{mid}^2 / \sigma$  (see the inset of Figure 5a for a sketch with  $D_{mid}$ ). Other definitions of the Bond number have been proposed.<sup>41,42</sup> Here, a power law fit is obtained with  $T_r \propto Bo_m^{-0.46}$  and a coefficient of determination of 0.92. This results in  $T_r$  being proportional to  $R_{mid}^{-0.92}$ . For  $\bar{V} = 1$ , it was reported that  $T_r$  decreases linearly with  $Bo$  (see Figure S1b in the Supporting Information). However, when  $\bar{V} \neq 1$ , the curvatures controlling the Laplace pressures are changed, while the height,  $L_0$ , and thus the hydrostatic pressure, is not. Hence, a physics-based formulation for the Bond number would be

$$Bo^* = \frac{\rho g L_0}{\sigma / R_{mid} + \sigma / \mathcal{R}}$$

$\mathcal{R}$  is the radius in the vertical plane (see the sketch in the inset of Figure 5a), axisymmetric as a first approximation. As  $\sigma / \mathcal{R}$  changes sign when  $\bar{V}$  varies around 1,  $Bo^* \simeq \rho g L_0 R_{mid} / \sigma$ . Our results on  $Bo_m$  convert into  $T_r$  being close to a linear decrease with  $Bo^*$ , rather than  $Bo$ .

## CONCLUSIONS

Liquid transfer for viscoelastic polymer solutions was studied experimentally. Reference results using Newtonian liquids on the effect of the initial and final aspect ratios have shown a



**Figure 5.** (a)  $T_r$  as a function of  $\bar{V}$  for Newtonian and viscoelastic solutions. Liquid bridges formed in between two disks having  $R_0 = 2$  mm are stretched from  $L_0/R_0 = 0.66$  to  $L/R_0 = 2$  at  $U = 0.134$  m/s. The liquid volume introduced is varied from 8 to 20  $\mu\text{L}$  ( $0.5 < \bar{V} < 1.25$ ), as illustrated in the inset. (b)  $T_r$  as a function of  $Bo_m$  for PEO1000 over a range of  $R_0$  and  $\bar{V}$ . The trend line is a power law fit with  $T_r \propto Bo_m^{-0.46}$ . The photographs depict stretched liquid bridges for various  $\bar{V}$  with  $R_0 = 3$  mm, when the top disk reaches  $L/R_0 = 2$ , with arrows indicating the associated data points.  $\bar{V} = 1$  for the points from Figure S1.  $U = 0.08$  m/s, except for data from Figure 5a.

linear decrease of transfer ratio. Then, the cylindrical-shaped liquid capillary bridge, with pinned contact lines between two parallel disks, was stretched for a range of polymer mass fractions. The transfer ratio decreases with Deborah number and can be explained by the gravitational draining enhanced by the delayed filament thinning. The gravitational influence was further studied by using different disk radii, and the results show that transfer ratio decreases for viscoelastic fluids with increasing disk radius, similar to Newtonian fluids. From the printing point of view, smaller values of polymer mass fraction, disk radius, and initial stretching height along with final stretching height should be favored for larger liquid transfer. For non-cylindrical-shaped bridges, the liquid transfer behavior varies sensitively with the liquid volume introduced. Moreover, the behavior of the transfer for Newtonian solutions increases as a function of actual liquid volume introduced and decreases with viscoelastic solutions. Then, the trend for results with PEO1000 follows a power law with  $Bo_m^{-0.46}$ , where  $Bo_m$  is the Bond number computed from the initial mid-plane radius. Another Bond number,  $Bo^*$ , with explicit curvatures could be used but can have negative values. Hence, for future studies on transfer ratio, the experimentally tractable  $Bo_m$  based on actual radius  $R_{mid}$  is suggested.

## ■ ASSOCIATED CONTENT

### SI Supporting Information

The Supporting Information is available free of charge at <https://pubs.acs.org/doi/10.1021/acs.langmuir.1c01462>.

Details of the fluid properties including dimensionless numbers and additional results on  $T_r$  for effect of  $R_0$  and  $Bo$ ; effect of initial aspect ratio,  $L_0/R_0$ ; effect of final aspect ratio,  $L/R_0$ ; and effect of stretching velocity (PDF)

## ■ AUTHOR INFORMATION

### Corresponding Author

Jorge Peixinho – Laboratoire PIMM, CNRS, Arts et Métiers Institute of Technology, Cnam, Paris 75013, France; LOMC,

CNRS and Université Le Havre Normandie, Le Havre 76600, France; [orcid.org/0000-0003-0850-3406](https://orcid.org/0000-0003-0850-3406); Email: [jorge.peixinho@ensam.eu](mailto:jorge.peixinho@ensam.eu)

## Authors

Hrshikesh Pingulkar – LOMC, CNRS and Université Le Havre Normandie, Le Havre 76600, France

Olivier Crumeyrolle – LOMC, CNRS and Université Le Havre Normandie, Le Havre 76600, France

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## Notes

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